

SIMULATED TRANSPORT OF JET FUEL LEAKING INTO GROUND WATER, SINDH PAKISTAN

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Abstract: A three-dimensional model of the contaminant transport was developed to predict the fate of jet fuel, which leaked from the above surface storage tanks in the urban site of Karachi, Pakistan. Since the tanks were situated in a sandy layer, the dissolved product entered the ground water system and started spreading beyond the site. The modeling process comprised the steady-state simulation of the ground water system, the transient simulation of the ground water system in the period from January 1986 through December 2073, and the calibration of jet fuel that was performed in context of different parameters in the groundwater system. The fuel was simulated using a modular three-dimensional finite-difference groundwater model (PMWIN) ModFlow and a solute transport model (MT3D) in the 1986-2001 periods under a hypothetical scenario. After a realistic distribution of piezometric heads within the aquifer system, calibration was achieved and matched to known conditions; the solute transport component was therefore coupled to the flow. Jet fuel concentration contour maps show the expanding plume over a given time, which becomes almost prominent in the preceding years.

Keywords: calibration, contaminant plume, jet fuel, Pakistan, solute transport model

Introduction:

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Ground water is a major source for domestic and industrial uses in many urban settlements of the world. Effluents from industrial areas as well as accidental spills and leaks from surface and underground storage tanks are the main sources of natural ground water contamination. When such contamination is detected, it becomes essential to estimate the spatial extent of contamination. Conventionally, determination of the extent of contamination is undertaken by collecting many samples within time and budgetary constraints from

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several points, which in general requires the installation of several observation wells. As a result, the cost of such operations can be very high, especially when measurements with higher resolution are required.

Two-dimensional (2-D) solute transport models can be used to predict the effects of transverse dispersion of the contaminant plume (spreading). Additionally, 2-D models are appropriate where the contaminant source may lie within or near the radius of influence of a continuously pumping well. While three-dimensional (3-D) numerical models should only be used if extensive data are available regarding vertical and horizontal heterogeneity, and spatial variability in contaminant concentrations. A localized contaminant transport model for groundwater is developed to gain insight into the dynamics of the leakage of jet fuel from above-ground storage tanks in the metropolitan area of Karachi, Pakistan. The jet fuel consists of refined, kerosene-type hydrocarbons, which are mixtures of benzene, toluene, ethyl benzene, and isomers of xylene (Kim and Corapcioglu 2003). Hypothetical monitoring wells were established to estimate the concentrations of jet fuel over a stipulated time period as a result of continuous seepage from the storage depot. Although, no specific data on the history of seepage were available, in view of the results inferred from an electrical resistivity sounding survey (ERSS) coupled with the findings of previous investigators from (Mott MacDonald Pakistan [MMP] 2000) it is envisaged that seepage from the storage tanks occurred for more than a decade. MMP 2000 conducted the study on soil and ground water assessment of environmental damage due to oil pollution and remedial measures were suggested for depots / installations / airfields of Shell Pakistan, scattered throughout the country. The Table 1 provides the composition of jet-fuel (Annexes).

Literature Review

Kim and Corapcioglu (2003) developed a two-dimensional model to describe areal spreading and migration of light nonaqueous-phase liquids (LNAPLs) introduced into the subsurface by spills or leaks from underground storage tanks. The nonaqueous-phase liquids (NAPL) transport model was coupled with two-dimensional contaminant transport models to predict contamination of soil gas and ground water resulting from a LNAPL migrating on the water table. Simulations were performed using the finite-difference method to study LNAPL migration and ground water contamination. The model was applied to subsurface contamination by jet-fuel. Results indicated that LNAPL migration was affected mostly by volatilization. Further, the spreading and movement of the dissolved plume was affected by the geology of the area and the free-product plume. Most of the spilled mass remained as a free LNAPL phase 20 years after the spill. The migration of LNAPL for such a long period resulted in the contamination of both ground water and a large volume of soil.

El-Kadi (2007) investigated the US Navy's bulk fuel storage facility at Red Hill located on the island of Oahu. The facility consisted of 20 buried steel tanks with a capacity of about 12.5 million gallons each. The tanks contain jet-fuel and marine diesel fuel. The bottoms of the tanks are situated about 80 feet above the basal water table. The geology of the area is primarily basaltic lava flows. Investigations found evidence of releases from several tanks. Two borings were drilled to identify and monitor potential migration of contamination to the potable water source. A numerical model of the regional hydrogeology at the Red Hill Fuel Storage Facility (RHFSF) was developed to simulate the fate and transport of potential contamination from the jet-fuel tanks and the effect on the saltwater/freshwater transition zone of various pumping scenarios.

Periago et al. (2000) investigated infiltration into soil of contaminants present in cattle slurry. Column experiments were performed in order to characterize the release

of contaminants at the slurry-soil interface after surface application of slurry with subsequent rainfall or irrigation. The shape of the release curves suggests that the release of substances from slurry can be modeled by a single-parameter release function. They compared prediction of solute transport (a) with input defined by the release function and (b) assuming rectangular-pulse input.

Eric et al. (1986) developed a parameter identification (PI) procedure and implemented with the United States Geological Survey's Method of Characteristics (USGS-MOC) model. The test results showed that the proposed algorithm could identify transmissivity and dispersivity accurately under ideal situations. Because of the improved efficiency in model calibration, the extended application to field conditions was effective.

Jin et al. (2008) investigated hydrocarbon plumes in ground water through the installation of extensive monitoring wells. Electromagnetic induction survey was carried out as an alternative technique for mapping petroleum contaminants in the subsurface. The surveys were conducted at a coal mining site near Gillette, Wyoming, using the EM34-XL ground conductivity meter. Data from this survey used to validate with the known concentrations of diesel compounds detected in ground water. Ground water data correlated perfectly with the electromagnetic survey data, which was used to generate a site model to identify subsurface diesel plumes. Results from this study indicated that this geophysical technique was an effective tool for assessing subsurface petroleum hydrocarbon sources and plumes at contaminated sites.

Materials and methods:

Site Description

The project site is located between longitudes 67° 07' 20" and 67° 10' 30" and latitudes 24° 52' 20" and 24° 54' 20". The land surface elevation ranges from

approximately 50 to 109 ft (15 to 33 m) above mean sea level (AMSL). In the far south, the Malir River drains into the Arabian Sea (Fig. 1). The typical lithology of the site is silty to sandy clay from 0 to 15 ft (4.6 m) bls (below land surface), gravelly sand from 15 to 43 ft (4.6 to 13 m) bls, and clayey to silty sand from 43 to 80 ft (13 to 24 m) bls. The region is arid with an average annual rainfall of about 200 mm (7.9 in.). Out of this, only 10 % (Arshaf and Ahmad 2008) is considered to recharge the aquifer system (6.34×10^{-9} m/sec).

The vadose zone is contaminated with up to 1300 ppm of total petroleum hydrocarbons (TPH) within the storage site. In the previous study by (Mott MacDonald Pakistan [MMP] 2000), soil samples were collected from different locations with 3 feet (1 m) bls and analyzed to estimate the concentration of hydrocarbon compound. Soil samples associated with the storage area have indicated higher TPH concentrations. The contaminant plume follows the hydraulic gradient to the southwest.

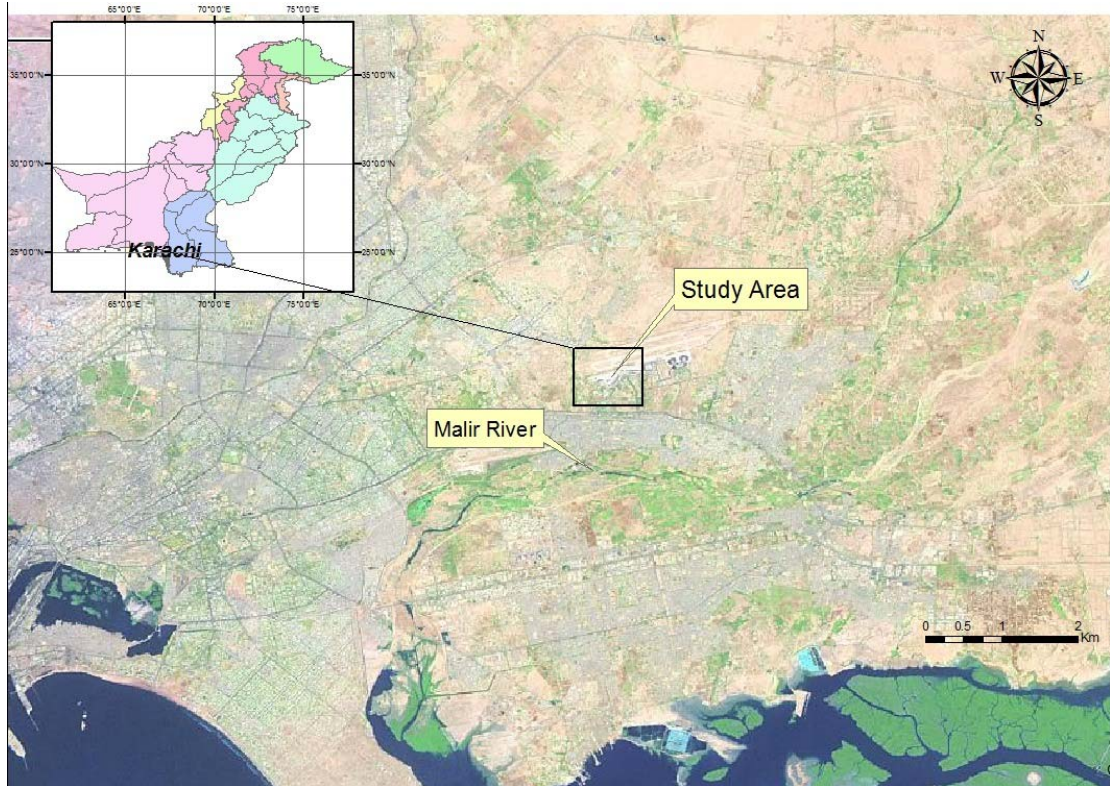
Conceptual Model

The groundwater flow system is treated as a two layer. The upper layer (predominantly silty sand) is bounded above by the water table and is 15 ft (4.6 m) thick, while the lower layer (predominantly clayey sand) is 65 ft (20 m) thick. These are unconfined and recharged from the surface by infiltrating rain, but only over permeable surfaces. A small stream which runs along east of model area acts as a drain to groundwater, which flows from the northeast to the southwest. With the exception of the stream, all other boundaries are artificial, that is neither constant head, nor constant flow boundaries. The processes that control the groundwater flow are:

- (i) recharges from infiltrated rainfall;
- (ii) flow entering the model across the eastern boundary (also across the northern boundary);
- (iii) flow reaching the stream;

- (iv) flow leaving the model across the southern boundary; and pumping from one well near tank no. 9.

Figure no. 1 Location of the study area



Values of hydraulic conductivities (K) for the layers are taken from the literature (Fetter 2000). The K value for depth range 16-31 ft (4.9-9.4m) is taken as 1.7×10^{-6} ft/sec (5.2×10^{-7} m/sec) and for depth range 31-97 ft (9.4-30 m) as 1.5×10^{-5} ft/sec (4.6×10^{-6} m/sec).

The transport and fate of hydrocarbons depend on multi-physical and chemical processes, including advection, dispersion, volatilization, dissolution, biodegradation, and sorption. When a solute undergoes chemical reactions, its rate of movement may be substantially less than the average rate of ground water flow. In this study, retardation of the movement of dissolved hydrocarbons is simulated as a sorption process, which includes both adsorption and partitioning into soil organic matter or organic solvents.

The MT3D software used for this simulation (Zheng 1990) uses a linear isotherm to simulate partitioning of a contaminant species between the porous media and the fluid phase due to sorption. This sorption process is approximated by the following equilibrium relationship between the dissolved and adsorbed phases:

$$S = K_d C$$

Where S is the concentration of the adsorbed phase (M/M), C is the concentration of the dissolved phase (M/L^3) and K_d is the sorption or distribution coefficient (L^3/M). K_d values for organic materials are commonly calculated as the product of the fraction of organic carbon in the soil, f_{oc} , and the organic carbon

partitioning coefficient, K_{oc} , or $K_d = f_{oc} K_{oc}$. K_{oc} values are contaminant specific and reported in various sources (Key 1997; Jeng et al. 1992; EPA 1989; ASTM 1995). The f_{oc} in the uncontaminated soil was estimated to range from 0.001 to 0.02 based on guidance by Newell et al. 1996. Assuming the linear isotherm, the retardation factor (R) is expressed as follows:

$$R = 1 + (r_b/n_{eff}) K_d$$

where r_b is the bulk density of the porous material (M/L^3) and n_{eff} is the effective porosity.

For jet fuel, the distribution coefficient K_d is taken as $0.004415 \text{ ft}^3/\text{kg}$. With these values,

$$R = 1 + [(48 \text{ kg}/\text{ft}^3)/0.25] \times 0.004415 = 1.848 \text{ (Kim and Corapcioglu 2003)}$$

Numerical Ground Water Flow Modeling

Processing ModFlow for Windows (PMWIN5), a modular 3-D finite-difference groundwater model, is used to configure the flow field (McDonald and Harbaugh 1988). The model consists of 41 columns and 39 rows in each layer (Fig. 2). The size of cells is $410 \text{ ft} \times 410 \text{ ft}$ ($125 \text{ m} \times 125 \text{ m}$) outside the fuel storage domain and $205 \text{ ft} \times 205 \text{ ft}$ ($62.5 \text{ m} \times 62.5 \text{ m}$) within the storage domain.

Automatic calibration of the water table was made with algorithm - UCODE and a perfect match obtained with the known condition prior to developing the transport model (Poeter and Hill 1998, 1999). Using the steady-state hydraulic heads calculated by PMWIN5 as the initial condition, the solute transport model MT3D was run to simulate the dispersion of the dissolved jet-fuel plume (Zheng 1990).

The parameters adjusted were the retardation factor R for each cell within the finite-difference grid, and the dispersion coefficient. Concentration-time curves have been calculated for ten monitoring wells. PMPATH (Chiang and Kinzelbach 1998) is used to retrieve the ground water flow model

and simulation result from PMWIN5. A semi-analytical particle-tracking scheme is used to calculate the ground water flow paths, travel times, and time-related capture zones resulting from pumping a neighboring well at the storage facility (Pollock 1989).

As a preprocessor to modeling and creating input data files, the PMWIN5 utility package was used. Prior to initiating the modeling work, a ground water information system was established with all data in binary and / or ASCII files that could be exported to other software.

Exploration Program (Hypothetical)

The dissolved phase jet-fuel plume was traced using a combination of ten hypothetical monitoring wells (Fig. 2) known as MW-1 through MW-10. The wells served to identify lithology, observe water levels, and monitor concentrations of organic compounds. The wells extend to a depth of 80 ft (24 m). In addition, the actual well was completed to a depth of 100 ft (30.5 m) near storage tank no.9 in case of emergency need. In the modeling study, this well was used to track the time-related capture zone. The general layout of the storage tanks over the finite-difference grid is shown in Fig. 3. The location of the pumping well is marked as a small red square in Fig. 2 and Fig. 3.

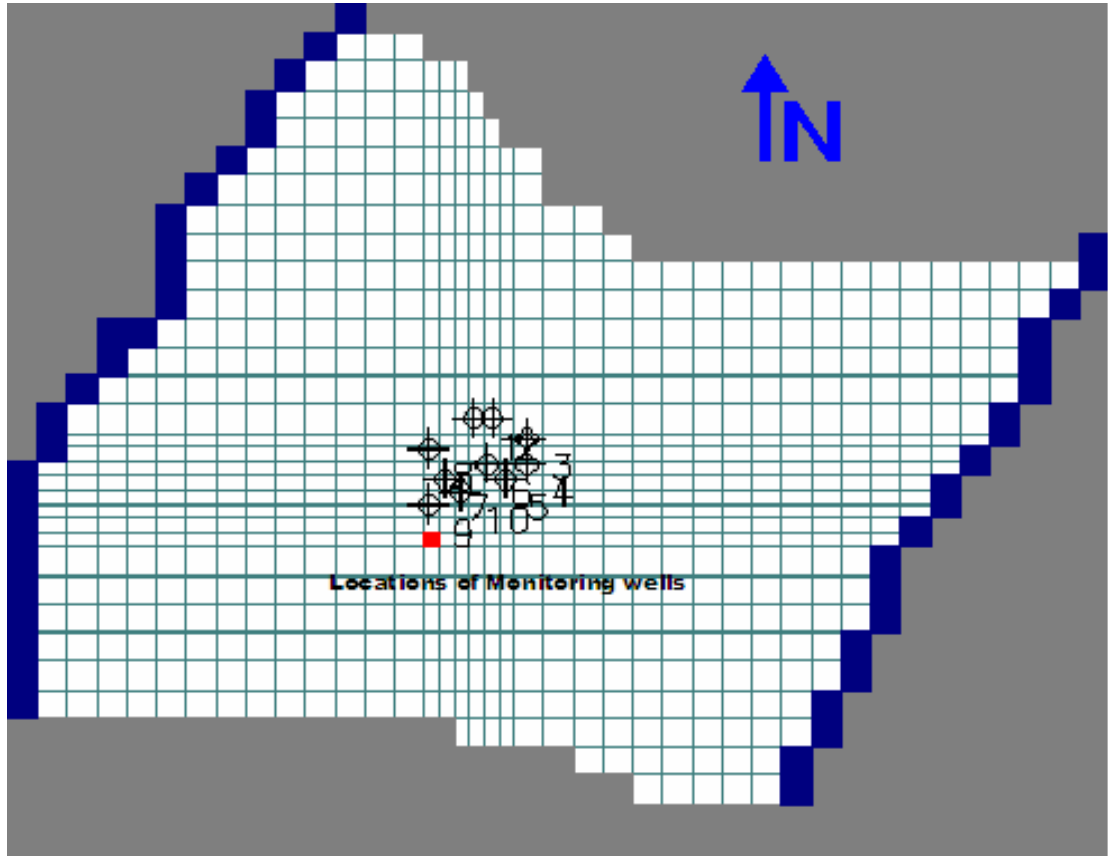
Model Calibration

The model was calibrated for steady-state conditions. Since it was speculated that the seepage of the fuel might have started as early as 1986, simulation of the ground water flow was begun in January 1971, the opening of storage facility. In the steady-state phase the only input comes from constant head boundaries (along the east and west of the model) and from infiltrated rainfall.

All output goes into constant head boundaries (the stream and the southwest boundary of the model). The differences in the known and simulated heads were calibrated to less than 0.30 ft (0.091 m) by

making slight adjustments in the K values of both layers.

Figure no. 2 Model design indicating finite difference grid and locations of hypothetical monitoring wells



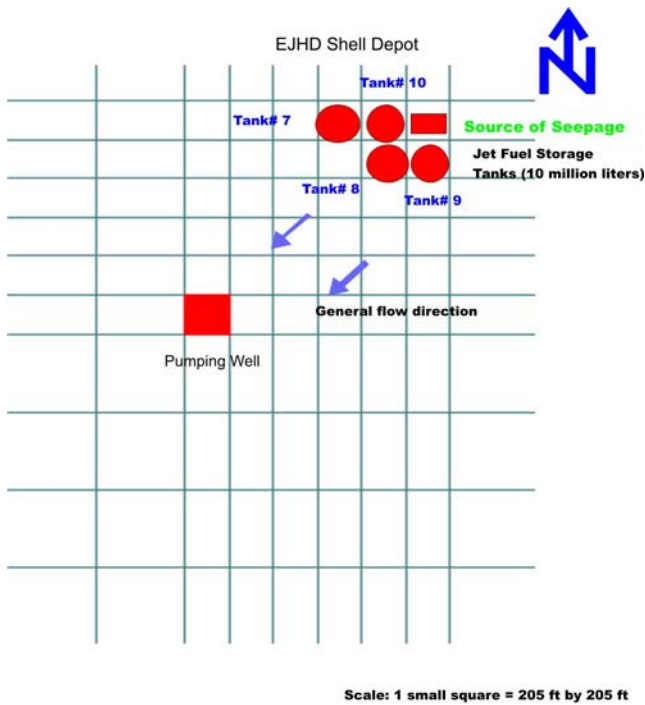
Transient calibration of ground water flow was accomplished using the time-variant hydraulic head values. Parameters such as recharge rates during each stress period, hydraulic heads in the stream, and along with the model boundaries, aquifer storage properties, pumping rates, and time-dependent capture zone were adjusted during the calibration.

To be objective and consistent, the recharge from infiltration was made equal to 10% of rainfall in each month. Effective porosity of the aquifer was varied between

15% and 25% until the value of 25% was determined to be the best predictor for the model. Constant pumping rates of 1500 US gallons/hr ($1.58 \times 10^{-3} \text{ m}^3/\text{sec}$) and 1000 US gallons/hr ($1.05 \times 10^{-3} \text{ m}^3/\text{sec}$) were used in layer 1 and layer 2 respectively.

The period from 1986 through 2000 was divided into seven stress periods, each of 2 years in duration. From 2000 to 2001, one stress period was assigned. The length of a stress period was made equal to the number of days in that month.

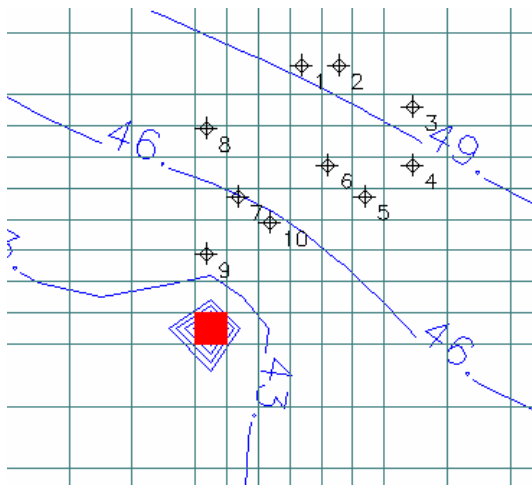
Figure no. 3 Layout of the storage tanks marked on a finite-difference grid



Results and discussion:

The effect of the pumping well is clearly visible as a cone of depression (Fig. 4). The drawdown was determined to be 14.0 ft (4.3 m) near the storage facility.

Figure no. 4 Cone of Depression visible around pumping well developed in layer 1



The model assumes uniform recharge from infiltrated rainfall to every “recharging” cell. Although effective porosity, hydraulic conductivity, and recharge may vary in space and time, the model is expected to have produced a reasonable configuration of the ground water flow pattern throughout the whole period of simulation. The time-related capture zones produced due to constant pumping are shown in Figs. 5 and 6. Water balances, which was calculated for each year of the simulated period, showed a perfect match between the input and output components.

Calibration of Plume Movement

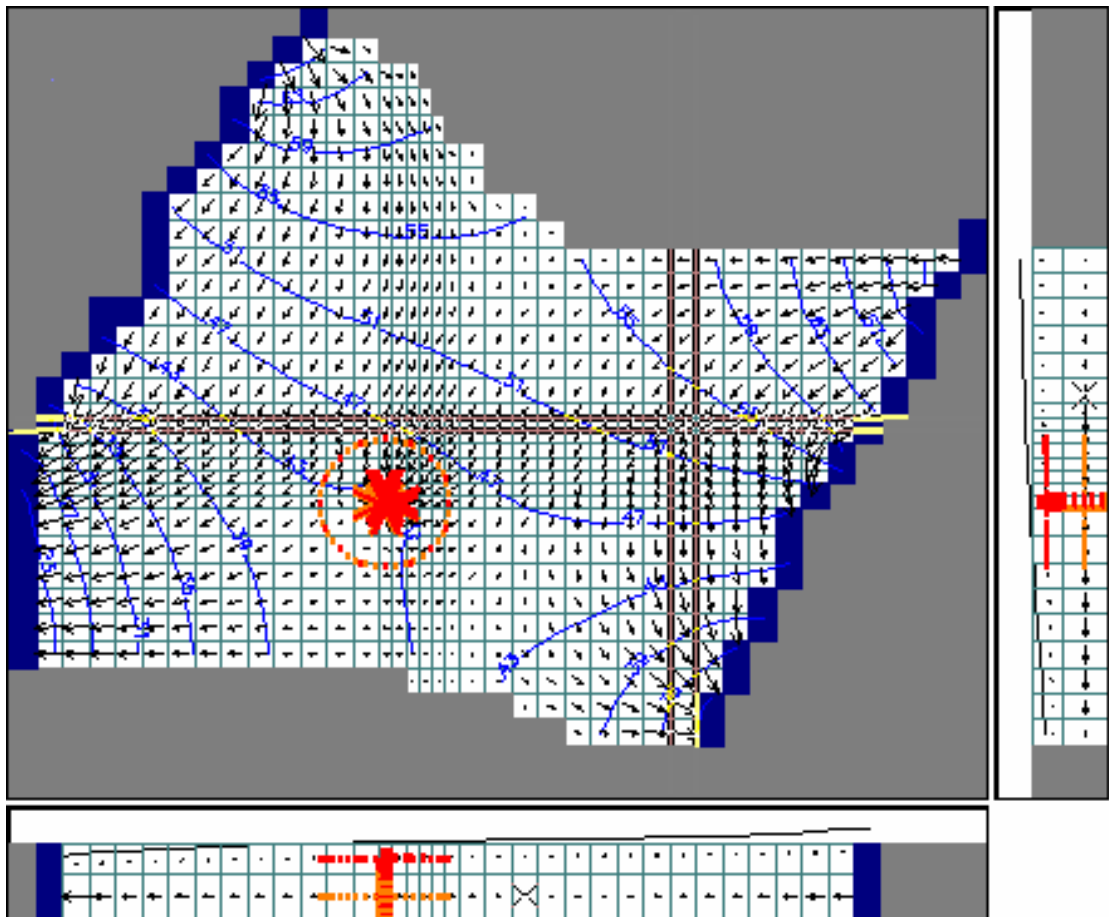
For simulation of the movement of dissolved jet fuel, lateral hydraulic conductivity values equal to 0.864 ft/day (0.263 m/day) for layer 1 and 1.29 ft/day (0.393 m/day) for layer 2 were accepted, while the vertical hydraulic conductivity ones were taken as 0.0864 ft/day (.0263 m/day) and 0.129 ft/day (.0393 m/day) for each layer, respectively (Fetter

2000). The hydraulic gradient and flow-net were obtained by running the flow component of the model derived from water level information in the previous study.

The United States Environmental Protection Agency (USEPA) and the Georgia Environmental Protection Division (GAEPD) recommend that the value for longitudinal dispersion should be one-tenth of the distance from the place where a contaminant enters the ground water system to the down-gradient receptor (a well,

stream, or other point of compliance). The distance from the storage facility (tank no. 7) to the pumping well is approximately 100 ft (30.48 m). In all calibration runs, as recommended, the value for longitudinal dispersion was set at 10 ft (3 m). USEPA and GAEPD also recommend for a solute transport model that the value for transverse dispersion equal one-third of the longitudinal dispersion.

Figure no. 5 Capture zone of the pumping well with arrows indicating flow directions



For this model, transverse dispersion would equal 3.3 ft (1.0 m). In the simulation of the fate of jet fuel, the transverse dispersion coefficient was varied within a range of 2.0 ft to 3.3 ft (0.61 m to 1.0 m). In

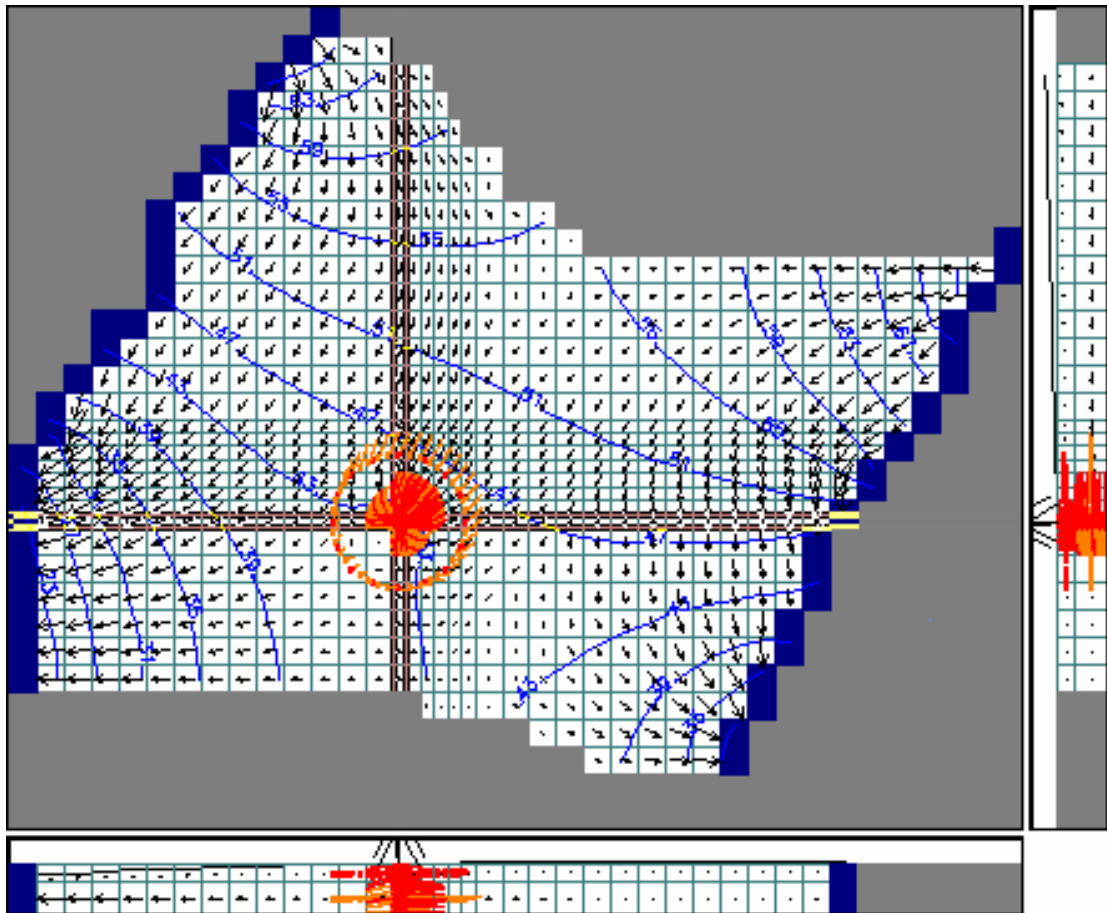
the model a value of $0.001 \text{ ft}^2/\text{day}$ ($1 \times 10^{-5} \text{ cm}^2/\text{sec}$) was used for molecular diffusion.

With a retardation factor of 1.80, the dissolved jet fuel takes 1.33 years to travel a lateral distance of about 70 to 80 ft (21 to 24

m) in ground water beneath tank no. 8. The best value of the microbial decay coefficient for jet fuel is estimated to be 1^{-10} / day with a

microbial yield coefficient for oxygen of 0.52 (Fetter 2000).

Figure no. 6 500-day-capture zone calculated by PMPATH



Strategy Development for Release of Jet Fuel

The previous integrity test run on the storage tanks containing 10 million litres of jet fuel indicated no loss. The date when the leak initially began is unknown, although inventory records indicated that the leak was not present before the tank integrity testing. The product has been detected in several hypothetical-monitoring wells (notably in MW-2 and MW-4) and in many soil samples taken within several tens of feet of the tank (McDonald and Harbaugh 1988). The initial

concentration of jet fuel entering the system is not of prime concern for the modeling.

The product of the influx (in L^3/T) and the concentration (in M/L^3) gives the total mass of jet fuel entering the system in a certain time interval. For the purpose of calibrating the jet fuel input, the initial concentration used, based upon field data (Mott MacDonald Pakistan [MMP] 2000), varied from 0.095 to 0.19 g/ft^3 (0.0027 to 0.0054 g/m^3). The initial mass of jet fuel, as simulated by the model, was equal to each of four cells “injecting” at a mass rate of 95 to 190 g/ft^3 (2.7 to 5.4 g/m^3) following the

initial period of 15 years during which no ground water contamination was assumed (Tab. 2).

Table no. 2 Strategy developed for the plume modeling scenarios

Phase	Stress period	Condition
Safe Period	15 years (1971 to 1986)	No leakage
Hazardous Period	10 years (1986 to 1996)	Low to moderate leakage
Risk Assessment	5 years (1996-2001)	Moderate leakage
Future Prediction	10 years (2001 – 2011)	Accretion in leakage

Using steady-state hydraulic heads as initial conditions, the evolution of the plume was modeled over nine stress periods as a result of continuous seepage from cells (18, 16, 1; tank 7), (19, 16, 1; tank 10), (19, 17, 1; tank 8), and (20, 17, 1; tank 9) as shown in Table 3.

Table no. 3 Stress period used in time-dependent solute transport modeling of jet fuel

Stress Period	Time interval (years)	Elapsed Time (secs)	Period
1	2	6.30×10^7	1986 - 88
2	2	12.60×10^7	1988 - 90
3	2	18.92×10^7	1990 - 92
4	2	25.23×10^7	1990 - 94
5	2	3.15×10^8	1994 - 96
6	2	3.78×10^8	1996 - 98
7	2	4.41×10^8	1998 - 00
8	1	4.73×10^8	2000 - 01
9	10	2.74×10^9	2001 - 11

Calibration Scenario

Parameters describing various processes are used after calibration with different combination of parameters (Tab. 4).

The release of the jet fuel is simulated in four cells, all along columns 18 to 20 from row 16 to row 17. The area of injection is equal to 42025 ft² (3,904 m²).

The concentration of jet fuel at the source (95 to 190 mg/ft³ [2.7 to 5.4 g/m³]) maintained constant throughout the designated “hazardous period” simulation period (1986-1996). The concentration was

slightly increased (about 0.01 %) from 1996 through 2001 and further up to longer time duration of 10 years i.e., 2011. The plume simulations are shown in Fig. 7. The jet-fuel break-through curves for the hypothetical monitoring wells are shown in Fig. 8. Conventionally, determination of the extent and level of contamination is undertaken by taking multiple measurements in wells (Zhou 1996; Plus and Paul 1997; Fisher and Goodman 2002). However, higher spatial resolution generally requires installation of monitoring wells, which is costly (Zeru 2004).

Table no. 4 Preliminary and final values of parameters used in modeling

Parameters	Value
Longitudinal Dispersion	10 ft
Transverse Dispersion	3.3 ft
Molecular Diffusion	0.001 ft ² /day
Distribution Coefficient	0.004415 ft ³ /kg
Retardation Factor (R)	1.80 to 1.848
Decay Coefficient	1 x10 ⁻⁹ day ⁻¹
Hydraulic Conductivity K (Layer-1)	1x10 ⁻⁵ ft/sec (0.864 ft/day)
Hydraulic Conductivity K (Layer-2)	1.49x10 ⁻⁵ ft/sec (1.29 ft/day)
Effective Porosity (Layer-1)	0.25
Effective Porosity (Layer-2)	0.30

Figure no. 7 Simulated Jet-fuel plumes (1986 to 1988 and 1988 to 1990)

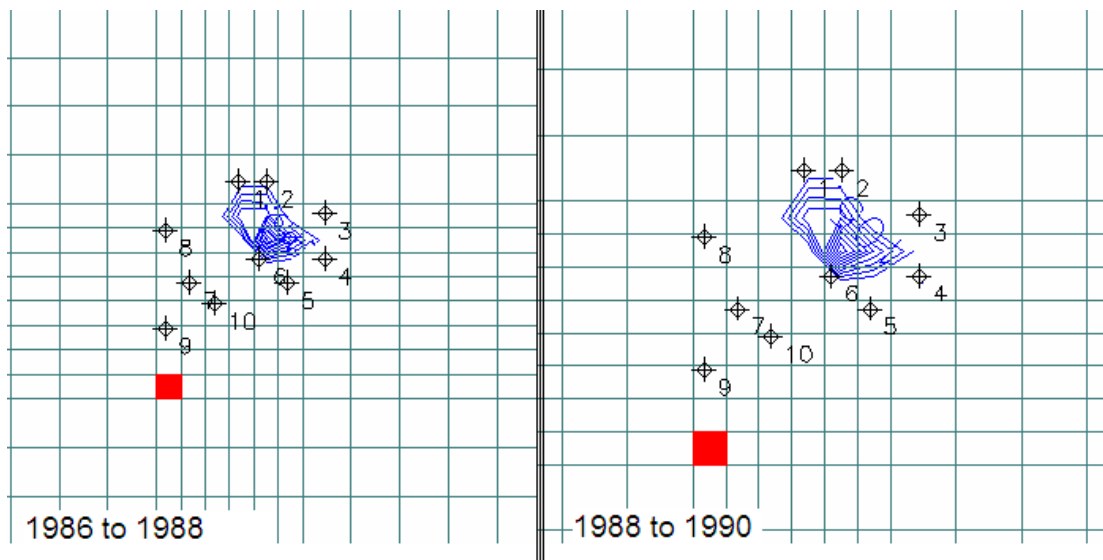
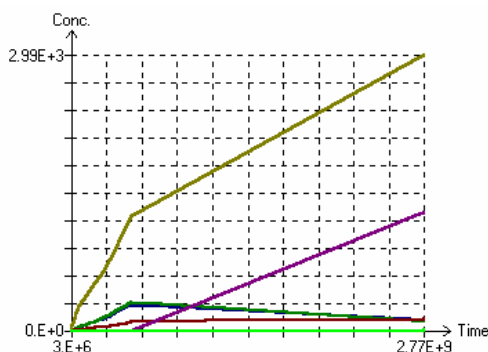


Figure no. 8 Concentration versus time based on data from 10 monitoring wells

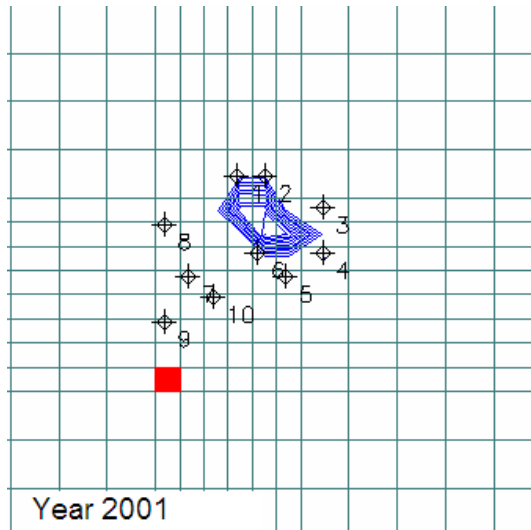


The modeled concentration at MW-1, MW-2, and MW-6 was much higher than the concentrations in the remaining wells. The maximum level of concentrations recorded in MW-6 was 2990 µg/ft³. Fig. 9 reflects the plume spreading of year 2001.

The shape of the plume is elliptical, with the major axis in the direction of ground water flow. This shape results from advection and longitudinal dispersion. The lateral spread of the plume results from transverse dispersion and molecular diffusion. The upgradient spread of the plume results from molecular diffusion (Bauer et al. 2004; Bockelmann 2003). The

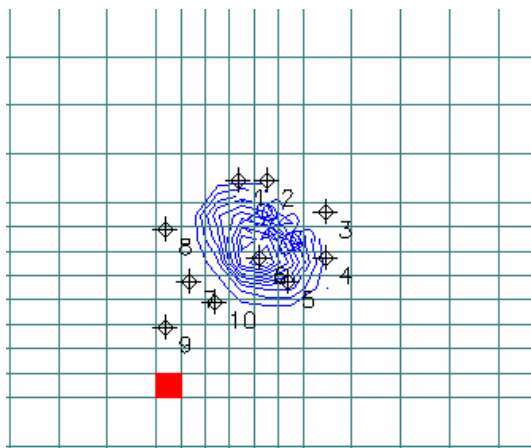
plume travels toward the stream, which is still far away in the west.

Figure no. 9 Extent of simulated plume in 2001



By the end of 2011, the effect of the plume becomes evident and the monitoring wells MW-4, MW-5, and MW-6 indicated increased concentration of jet fuel (Fig. 10). The resultant plume appears to be spreading more in the elliptical path but in the direction of ground water flow.

Figure no. 10 Extent of plume spreading in year 2011



Conclusions:

Based on the modeling, it is concluded that the jet-fuel plume has neither expanded nor moved considerably. It is less than 250 ft (76.2 m) beyond the storage tanks and is oriented northeast to southwest. The level of concentration found in the simulated monitoring wells is significant, but because ground water is brackish and thus unlikely to be used, no harmful effects are expected. An interdisciplinary investigation of the processes controlling the fate and the transport of hydrocarbons in the subsurface is needed.

Concentrations should be performed in wells within and down-gradient of the plume, as field data would help develop a stronger argument for the fate of jet fuel in ground water.

Rezumat:

SIMULAREA TRANSPORTULUI DE COMBUSTIBIL SCURS ÎN APA FREATICĂ ÎN ZONA SINDH PAKISTAN

Un model tri-dimensional al transportului de poluanți a fost dezvoltat pentru a prevedea soarta jetului de combustibil care se scurge de la rezervoarele de stocare de suprafață din zona urbană din Karachi, Pakistan. Din momentul când tancurile au fost plasate într-un strat de nisip, produsul dizolvat a intrat în sistemul apelor subterane și a început răspândirea dincolo de zona. Procesul de modelare cuprinde simularea stării de echilibru a sistemului de apă freatică, simularea tranzitorie a sistemului de apă freatică în perioada ianuarie 1986 până în decembrie 2073, precum și calibrarea jetului de combustibil, care a fost realizat în cadrul unor parametri diferiți din apele subterane ale sistemului. Combustibilul a fost simulat folosind un model modular tri-dimensional pentru apele subterane (PMWIN) ModFlow și un model de transport al soluției (MT3D) în perioada 1986-2001, în cadrul unui scenariu ipotetic. După o distribuție realistă a

capetelor piezometrice în cadrul sistemului acvifer, calibrarea a fost realizată și adaptată la condițiile cunoscute; componenta de transport a soluției a fost cuplată la curgere. Hărțile de contur a concentrației jetului de combustibil arată expansiunea penei într-un interval de timp dat, care devine aproape proeminentă în anii precedenți.

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Annexes:

Composition of Contaminant (Jet fuel)

Knowledge of the geochemistry of a contaminated aquifer is important to understand the chemical and biological processes controlling the migration of hydrocarbon contaminants in the subsurface. Originally, the jet fuel (kerosene oil) is the name assigned to a material with a biological origin, but now it is used to describe materials most of which contain carbon and hydrogen and which may contain oxygen, nitrogen, the halogens, and lesser amounts of other elements. The simplest of these are the hydrocarbons, molecules of hydrogen and carbon, many of which are the components of natural gas, petroleum, and coal. Petroleum, however, has a very large number of components ranging from methane to the high molecular weight materials asphalt and paraffin. Typical fractions into which crude oil is separated in an oil refinery and some principal molecular species are shown in [Table 1](#).

Table no. 1 The Fractions and Representative Components obtained from Crude Oil

Fraction from distillation	Boiling range	Product of secondary treatment	Typical molecular components
Gas	Below 20 °C	Gas Liquefied Pet. Gas (LPG)	CH ₄ methane, C ₂ H ₆ ethane C ₃ H ₈ propane, C ₄ H ₁₀ butane
Naphtha	20 - 175 °C	Naphtha gasoline	C ₁₁ H ₂₄ to C ₁₈ H ₃₈
Kerosene	175 - 400 °C	Kerosene diesel fuel Lubricating oil	C ₁₁ H ₂₄ to C ₁₈ H ₃₈ C ₁₅ H ₃₂ to C ₄₀ H ₈₂
Residue	above 400 °C	Asphalt	Heavier hydrocarbons